



Integrating Supercritical Carbon Dioxide Brayton Cycles into Concentrating Solar Power Plants

TM Hans, J van der Spuy & RT Dobson

^aSolar Thermal Energy Research Group (STERG), Stellenbosch University

^bCentre for Renewable and Sustainable Energy Studies (CRSES),

Stellenbosch University







CENTRE FOR RENEWABLE AND SUSTAINABLE ENERGY STUDIE



Contents

- Introduction
- S-CO₂ Brayton Cycles
- Properties of s-CO2
- S-CO₂ BC applicability to CSP
- Conclusion









Introduction

Greenhouse Gas Emissions



Google Public Data, 2018, World Development Indicators: Environment. Available at https://www.google.com/publicdata/explore?ds=d5bncppjof8f9 [Accessed 29/08/18]









Introduction

Electricity Production

- The energy sector is the largest contributor to GHG emissions: 84.5%
- 94% of electricity in South Africa produced from coal









Industry
Waste
Source: USAID, 2016, CHG Emissions in SA



Introduction

Mitigation target



Bischof-Niemz, 2017, Energy Modelling for South Africa, Latest Approaches & Results in a Rapidly Changing Energy Environment









Improved efficiency

- Large amounts of solar resource
- The most effective way to improve the CSP plant's efficiency is through improvements to the power cycle
- Efficiencies of over 50% possible in central receiver tower type CSP systems









Recuperated Recompression Cycle











Cooling











Specific Heat









Specific Heat









 $\langle \rangle \rangle$

Cooling process











Cooling process









 $\langle \rangle \rangle$

Compression

























Density









Compression









Compact turbomachinery



Wright, 2010, Operation and Analysis of a Supercritical CO2 Brayton Cycle







Recuperation











Heating



Thermal Conductivity

Expansion

CSP Plant Requirements

Temperature range

- Parabolic trough systems have concentration ratios of 80 and can reach temperatures of up to 400 °C.
- Central receiver power plants have ratios of up to 600 and can reach temperatures up to 1000 °C (Elsaket, 2007)
- Central receiver plants preferred

Temperature range

- Non-combustible
- No upper temperature limit
- Non-explosive
- Chemically stable
- Inexpensive
- Abundant

Pressure range

- Moderate pressure
- With pressures from the critical point of 7.38 MPa to around 20 MPa
- These pressures require sturdier components
- Seals and bearings

Central Receiver Plant Requirements 📀

Dry Cooling

- Dry-cooling reduces water consumption compared to wet cooling
- This is important as recent water shortages have demonstrated the scarcity of this resource in South Africa

Dry cooling

- Critical point ,31.1 °C, close to ambient temperature
- Must keep the inlet conditions pseudocritical
- Control system is important
- Dramatic changes in fluid properties near the critical point

Thermal Energy Storage

- Improved storage capacity
- Lower levelized cost of energy
- Controlled input
- Lower temperatures
- Higher efficiencies than steam

 \mathbf{C}

Direct heated closed loop cycle

- No use of fluids that are toxic, flammable, or have a high global warming potential
- Flexibility due to temperature range
- Stability in operation due to single phase
- Can place entire power cycle in the receiver

Overall size of power conversion system

Steam turbine

Source: Rochau, 2014, Commercializing the sCO2 Recompression Closed Brayton Cycle

Challenges for s-CO2 Brayton cycles ••

• Large shafts to transmit torque

Challenges for s-CO2 Brayton cycles ••

- Large shafts to transmit torque
- Large or expensive heat exchangers
- Specialised components such as bearings and seals
- Thermal stresses and fatigue failure
- Non-linearity of properties

Challenges for s-CO2 Brayton cycles •••

- Large shaft
- Large or ex
- Specialisec and seals
- Thermal str
- Non-linear

Flamant, 2013, Design of Compact Heat Exchangers for Transfer Intensification

Challenges for s-CO2 Brayton cycles ••

- Large shafts to transmit torque
- Large or expensive heat exchangers
- Specialised components such as bearings and seals
- Thermal stresses and fatigue failure
- Non-linearity of properties

Conclusion

- Increased electricity production
- Reduced investment costs
- Off design operation possible
- Better understanding of operation
- Quantifying the improvements
- There is still work to be done

ACKNOWLEDGEMENTS:

CONTACT DETAILS:

Taneha Mae Hans Solar Thermal Energy Research Group (STERG) Stellenbosch University South Africa

STERG@sun.ac.za +27 (0)21 808 4016

visit us: concentrating.sun.ac.za